

# Transient heat transfer measurements using thermochromic liquid crystal. Part 2: Experimental uncertainties

J. Michael Owen<sup>\*</sup>, Paul J. Newton, Gary D. Lock

*Department of Mechanical Engineering, University of Bath, Bath BA2 7AY, UK*

Received 28 January 2002; accepted 4 August 2002

## Abstract

In Part 1 of this two-part paper, an “exponential-series technique” was used to calculate heat transfer coefficient,  $h$ , for the so-called slow transient case where it is not possible to generate a step-change in the air temperature. Small uncertainties in the measured temperatures can, however, create large uncertainties in the calculated value of  $h$ , and the amplification parameter,  $\Phi_h$ , is defined as the ratio of the relative uncertainty in  $h$  to the relative uncertainties in the temperatures. Using an uncertainty analysis, theoretical expressions for  $\Phi_h$  are found for the slow transient case, and these expressions are in excellent agreement with values computed using a Monte Carlo method. The results provide guidance in the selection of design parameters for an experiment and for the calculation and minimisation of the uncertainty in  $h$ .

© 2002 Elsevier Science Inc. All rights reserved.

**Keywords:** Uncertainties; Transient heat transfer; Thermochromic liquid crystal

## 1. Introduction

Part 1 of this two-part paper (see Newton et al., 2003, which is referred to below as 1) describes the “exponential-series technique”. This technique can be used to determine the heat transfer coefficient,  $h$ , for “slow-transient” cases where it is not possible to generate a step-change in the air temperature.

Yan and Owen (2002) used the results of Coleman and Steele (1999) to provide an uncertainty analysis for heat transfer coefficients derived from the step-change solutions of Fourier’s equation. If the random uncertainties in the measured temperatures are known then the uncertainty in  $h$  can be readily determined. This enables the transition temperature of the thermochromic liquid crystal (TLC) to be chosen so as to minimise the uncertainty in  $h$ .

It should be pointed out that, like the exponential-series technique described in 1, the uncertainty analysis discussed below assumes that  $h$  is invariant with time. Whilst this may not always be true in practice, the

sensitivity of  $h$  to the (time-dependent) level or distribution of surface temperature can be tested by using two or more narrow-band liquid crystals to determine  $h$ .

It should also be pointed out that the uncertainty analysis assumes random uncertainties in the measured temperatures. Systematic uncertainties or biases (due, for example, to the calibration of the liquid crystal using the same thermocouple employed in the calibration of the air temperature) are beyond the scope of this paper.

The step-change analysis of Yan and Owen is extended below to the slow transient case. The uncertainties in  $h$  are quantified in Section 2, and Section 3 describes how to calculate the amplification parameters, which relate the uncertainties in  $h$  to those in the measured temperatures. The conclusions are summarised in Section 4. Using these results, experimenters should be able to quantify and to minimise the uncertainties in  $h$  resulting from the use of narrow-band TLC in slow-transient heat-transfer experiments.

## 2. Experimental uncertainties

The symbols used throughout this paper are defined in the Nomenclature of 1.

<sup>\*</sup> Corresponding author. Tel.: +44-01225-386-115; fax: +44-01225-386-928.

E-mail address: [j.m.owen@bath.ac.uk](mailto:j.m.owen@bath.ac.uk) (J.M. Owen).

### 2.1. Solution of Fourier's equation for the "exponential-series case"

For convenience, Eq. (2.22) of 1 is rewritten below as

$$\Theta = \frac{T_w - T_0}{T_{aw,\infty} - T_0} = \sum_{j=1}^m c_j g(\beta, \lambda_j), \quad (2.1)$$

where

$$\lambda_j = \frac{\beta}{\beta_{\tau,j}} = \sqrt{\frac{t}{\tau_j}}, \quad (2.2)$$

$$c_j = \frac{T_{a,j}}{\sum_{j=1}^m T_{a,j}} \quad (2.3)$$

and

$$g(\beta, \lambda_j) = 1 - \frac{\lambda_j^2}{\beta^2 + \lambda_j^2} [1 - f(\beta)] - \frac{\beta^2}{\beta^2 + \lambda_j^2} e^{-\lambda_j^2} \left[ 1 + \frac{\lambda_j}{\beta} \phi(\lambda_j) \right], \quad (2.4)$$

where  $f(\beta)$  is defined in Eq. (2.6) of 1 and

$$\phi(\lambda_j) = \frac{1}{\pi} \left[ \lambda_j + 2 \sum_{n=1}^{\infty} \frac{e^{-n^2/4}}{n} \sinh(n\lambda_j) \right]. \quad (2.5)$$

Fig. 1 shows the effect of  $\lambda$  (for the case where  $m = 1$  and  $\lambda = \lambda_1$ ) on the variation of  $\beta$  with  $\Theta$  according to Eq. (2.1). As  $\lambda \rightarrow \infty$ ,  $g(\beta, \lambda) \rightarrow f(\beta)$ ; that is, the step-change solution is the limit to the exponential solution. The two solutions are in close agreement for  $\lambda > 2.2$ .

As  $\beta \rightarrow \infty$ , Eq. (2.4) reduces to

$$g(\beta, \lambda_j) = 1 - e^{-\lambda_j^2}. \quad (2.6)$$

That is, as  $h \rightarrow \infty$ , the surface of the wall immediately reaches the instantaneous adiabatic-wall temperature.

### 2.2. Uncertainty in $h$

Consider the case where the random uncertainties in the measured values of  $T_w$ ,  $T_0$  and  $T_{aw}$  are independent of each other (as is often the case) then, using the method of Coleman and Steele (1999), it can be shown that

$$P_\beta^2 = P_\Theta^2 \left/ \left( \frac{\partial \Theta}{\partial \beta} \right)^2 \right., \quad (2.7)$$

where  $P_\beta$  and  $P_\Theta$  are the uncertainties in  $\beta$  and  $\Theta$ , respectively, and

$$P_\Theta^2 = \left( \frac{\partial \Theta}{\partial T_w} \right)^2 P_{T_w}^2 + \left( \frac{\partial \Theta}{\partial T_0} \right)^2 P_{T_0}^2 + \left( \frac{\partial \Theta}{\partial T_{aw}} \right)^2 P_{T_{aw}}^2, \quad (2.8)$$

where  $P_{T_w}$ ,  $P_{T_0}$  and  $P_{T_{aw}}$  are the respective uncertainties in the temperatures. It follows from the definition of  $\Theta$  that

$$P_\Theta^2 = \left[ \left( \frac{P_{T_w}}{\theta_{aw}} \right)^2 + (1 - \Theta)^2 \left( \frac{P_{T_0}}{\theta_{aw}} \right)^2 + \Theta^2 \left( \frac{P_{T_{aw}}}{\theta_{aw}} \right)^2 \right], \quad (2.9)$$

where

$$\theta_{aw} = T_{aw} - T_0. \quad (2.10)$$

It is assumed here that the relative uncertainties in  $t$  and  $\kappa$  are much smaller than those in  $h$ , so that

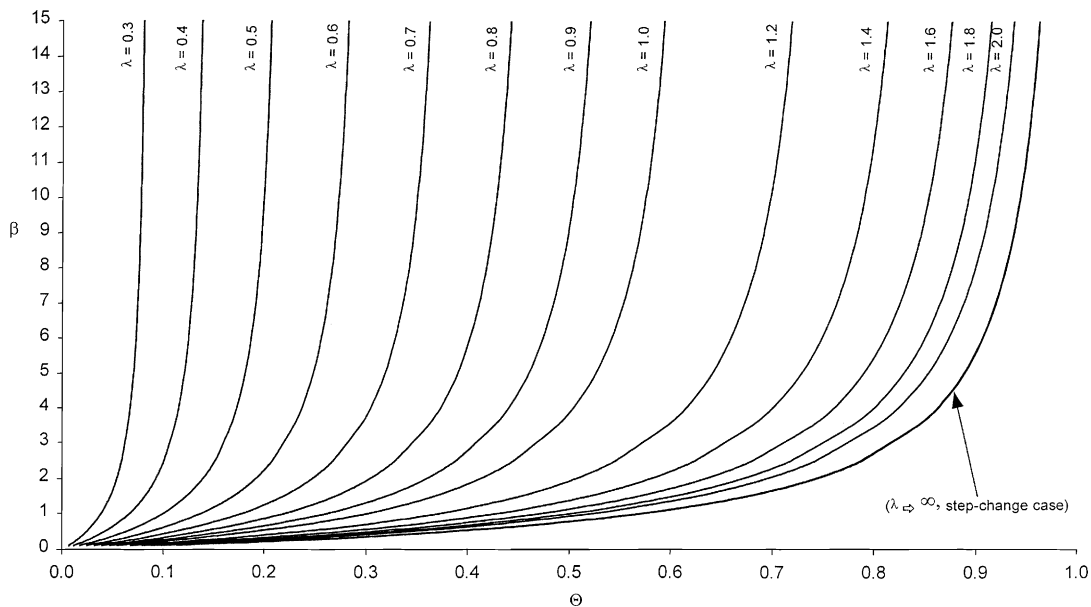


Fig. 1. Effect of  $\lambda$  on variation of  $\beta$  with  $\Theta$  for exponential case.

$$\frac{P_\beta}{\beta} \approx \frac{P_h}{h}. \quad (2.11)$$

(Although it may not be insignificant, an uncertainty in  $\kappa$  will produce a *bias*, or systematic error, in  $h$ , and this is beyond the scope of this paper.)

For convenience, let  $P_T$  be  $\max(P_{T_w}, P_{T_0}, P_{T_{aw}})$  so that Eqs. (2.7) and (2.9) can be expressed as

$$\frac{P_h}{h} = \frac{P_T}{\theta_{aw}} \left\{ \left( \frac{P_{T_w}}{P_T} \right)^2 + (1 - \Theta)^2 \left( \frac{P_{T_0}}{P_T} \right)^2 + \Theta^2 \left( \frac{P_{T_{aw}}}{P_T} \right)^2 \right\}^{1/2} \left/ \left( \beta \frac{\partial \Theta}{\partial \beta} \right) \right. \quad (2.12)$$

$\Theta$  and the uncertainties in temperature are taken to be known constants, so that the numerator of the RHS of Eq. (2.12) is invariant with time; the denominator, however, depends on  $h$  and  $t$ .

Following Yan and Owen (2002), an *amplification parameter*,  $\Phi_h$ , is defined as

$$\Phi_h = \frac{P_h}{h} \left/ \frac{P_T}{\theta_{aw}} \right. \quad (2.13)$$

From Eq. (2.12) it follows that

$$\Phi_h = \Gamma_\Theta \Gamma_\beta, \quad (2.14)$$

where

$$\Gamma_\Theta = \left\{ \left( \frac{P_{T_w}}{P_T} \right)^2 + (1 - \Theta)^2 \left( \frac{P_{T_0}}{P_T} \right)^2 + \Theta^2 \left( \frac{P_{T_{aw}}}{P_T} \right)^2 \right\}^{1/2} \quad (2.15)$$

and

$$\Gamma_\beta = \left( \beta \frac{\partial \Theta}{\partial \beta} \right)^{-1}. \quad (2.16)$$

A special case arises when the uncertainties in the temperatures are equal to each other so that  $P_{T_w} = P_{T_0} = P_{T_{aw}} = P_T$ . Denoting this case by  $*$ , Eq. (2.15) simplifies to

$$\Gamma_\Theta^* = \{2(1 - \Theta + \Theta^2)\}^{1/2} \quad (2.17)$$

and

$$\Phi_h^* = \Gamma_\Theta^* \Gamma_\beta. \quad (2.18)$$

As  $\Gamma_\Theta \leq \Gamma_\Theta^*$  for all  $\Theta$ , Eq. (2.18) provides an upper bound for the uncertainty in  $h$ .

Eq. (2.14) can be regarded as the general expression for  $\Phi_h$ . The actual value of  $\Phi_h$  depends on the relationship between  $\Theta$  and  $\beta$ , and the solutions for three cases are presented below.

### 3. Determination of amplification parameters

#### 3.1. Step-change case

It follows from Eqs. (2.5) and (2.6) in 1 that

$$\frac{\partial \Theta}{\partial \beta} = \frac{df}{d\beta} = 2[\beta(\Theta - 1) + \pi^{-1/2}]. \quad (3.1)$$

Hence, from Eqs. (2.14)–(2.16),

$$\Phi_h = \Gamma_\Theta / \{2\beta[\beta(\Theta - 1) + \pi^{-1/2}]\}, \quad (3.2)$$

which is the same as the result obtained by Yan and Owen (2002). It is interesting to note that, as  $\beta$  is uniquely related to  $\Theta$ ,  $\Phi_h$  for the step-change case is independent of  $h$ .

For the special case where the uncertainties in temperature are equal, Eq. (2.17) leads to the result that

$$\Phi_h^* = \frac{[(1 - \Theta + \Theta^2)]^{1/2}}{\sqrt{2}\beta[\beta(\Theta - 1) + \pi^{-1/2}]} \quad (3.3)$$

As  $\Phi_h \leq \Phi_h^*$ , Eq. (3.3) provides an upper bound for the amplification parameter.

The variation of  $\Phi_h^*$  with  $\Theta$  is shown in Fig. 2, and Yan and Owen found good agreement between Eq. (3.3) and computations made using a Monte Carlo method. A minimum value ( $\Phi_{h,\min}^* \approx 4.4$ ) occurs at  $\Theta \approx 0.52$ , and  $\Phi_h^* \lesssim 5$  for  $0.3 < \Theta < 0.7$ . In this range of  $\Theta$ , 1% uncertainty in the temperature measurement would cause around 5% uncertainty in the computed value of  $h$ , a result most experimenters would regard as acceptable.

#### 3.2. Exponential case

It follows from Eqs. (2.10) in 1 and (2.16) above that

$$\Gamma_\beta^{-1} = \beta \frac{\partial g}{\partial \beta}, \quad (3.4)$$

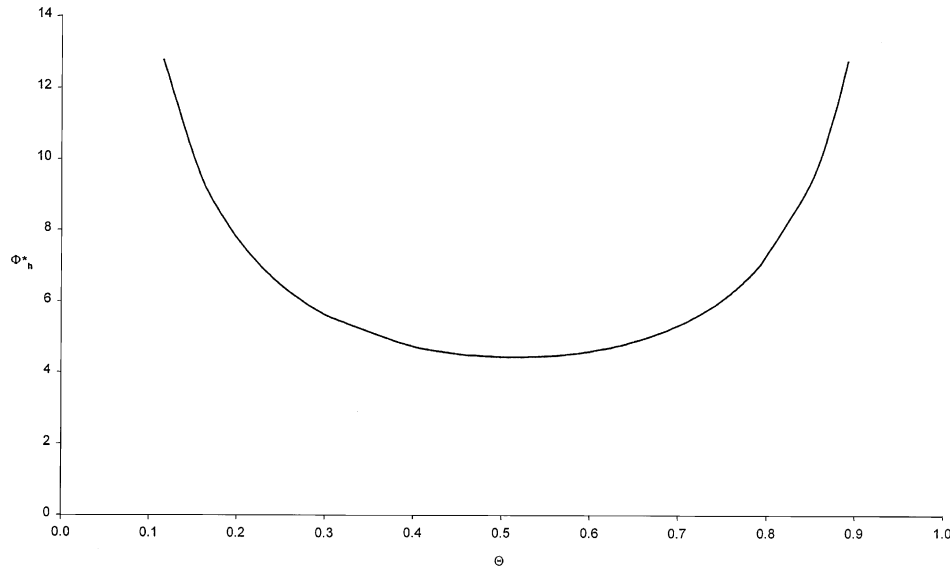
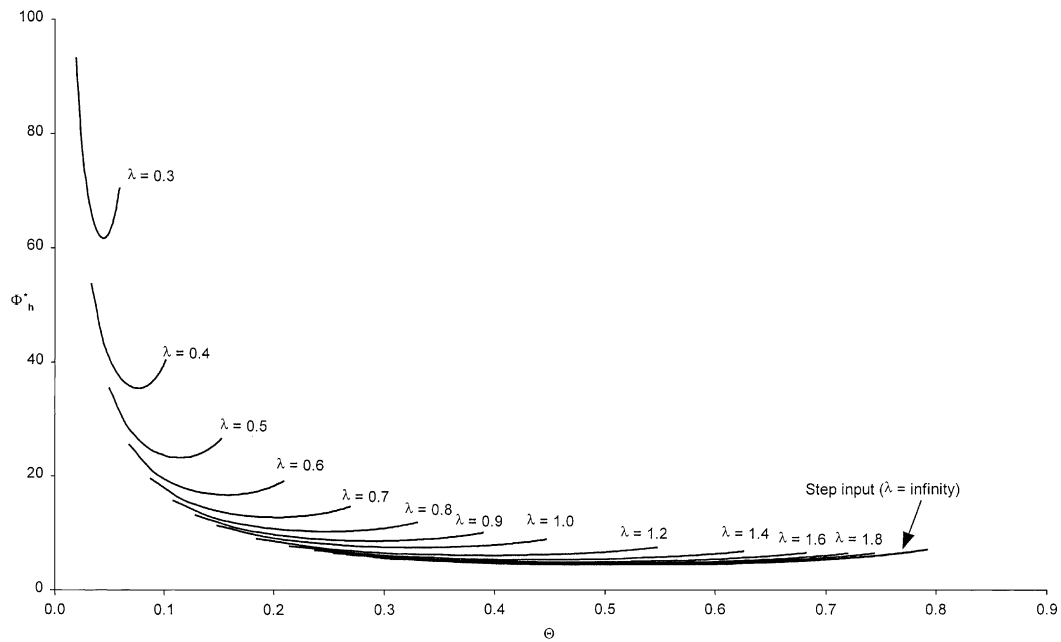
where it is assumed implicitly that there is no uncertainty in  $\lambda$ .

Hence, from the definition of  $g(\beta, \lambda)$  given in Eq. (2.4),

$$\Gamma_\beta^{-1} = \frac{\beta \lambda^2}{(\beta^2 + \lambda^2)^2} \left\{ 2\beta[1 - f(\beta)] + (\beta^2 + \lambda^2) \frac{df}{d\beta} - e^{-\lambda^2} [2\beta + (1 - (\beta/\lambda)^2) \lambda \phi(\lambda)] \right\}, \quad (3.5)$$

where  $df/d\beta$  is given by Eq. (3.1). Eq. (3.5) can be used with Eqs. (2.15) and (2.17) to calculate  $\Phi_h$  and  $\Phi_h^*$  according to Eqs. (2.14) and (2.18).

For the special case of equal uncertainties in the temperatures, the effect of  $\lambda$  on the variation of  $\Phi_h^*$  with  $\Theta$  is shown in Fig. 3. For  $\lambda > 2$ , it can be seen that  $\Phi_h^*$  for the exponential case tends to the value given by Eq. (3.3) for the step-change.

Fig. 2. Variation of  $\Phi_h^*$  with  $\Theta$  for step-change case.Fig. 3. Effect of  $\lambda$  on variation of  $\Phi_h^*$  with  $\Theta$  for exponential case.

In general,  $\Phi_h^*$  for the exponential case is larger than that for the step change and, for small values of  $\lambda$ , it can be very large. For example, for  $\lambda = 0.4$ ,  $\Phi_h^* > 35$ : 1% uncertainty in temperature results in more than 35% uncertainty in  $h$ . It is therefore desirable to make  $\lambda$  as large as practicable so as to reduce the uncertainty in  $h$ . For any value of  $\lambda$ , there is an optimum value of  $\Theta$  that will minimise  $\Phi_h^*$ , and this optimum value increases as  $\lambda$  increases: for  $\lambda > 2$ ,  $\Theta_{\text{opt}} \approx 0.52$ . As  $\tau$  is dependent on the experimental apparatus, the experimenter needs to

choose both  $\lambda$  and  $\Theta$  so as to achieve acceptably small values of  $\Phi_h^*$  for the duration of the experiment.

Fig. 4 shows the effect of  $\beta_\tau$  on the variation of  $\Phi_h^*$  with  $\Theta$  according to the equations derived above. In addition, computations were carried out using a Monte Carlo method (as described by Yan and Owen, 2002) in which random noise was added to  $T_w$ ,  $T_o$  and  $T_{\text{aw}}$ , and the associated values of  $h$  were computed using Eq. (2.1) (with  $m = 1$  and  $c_1 = 1$ ). A total of 10,000 values was used to calculate the average value of  $h$  and its uncer-

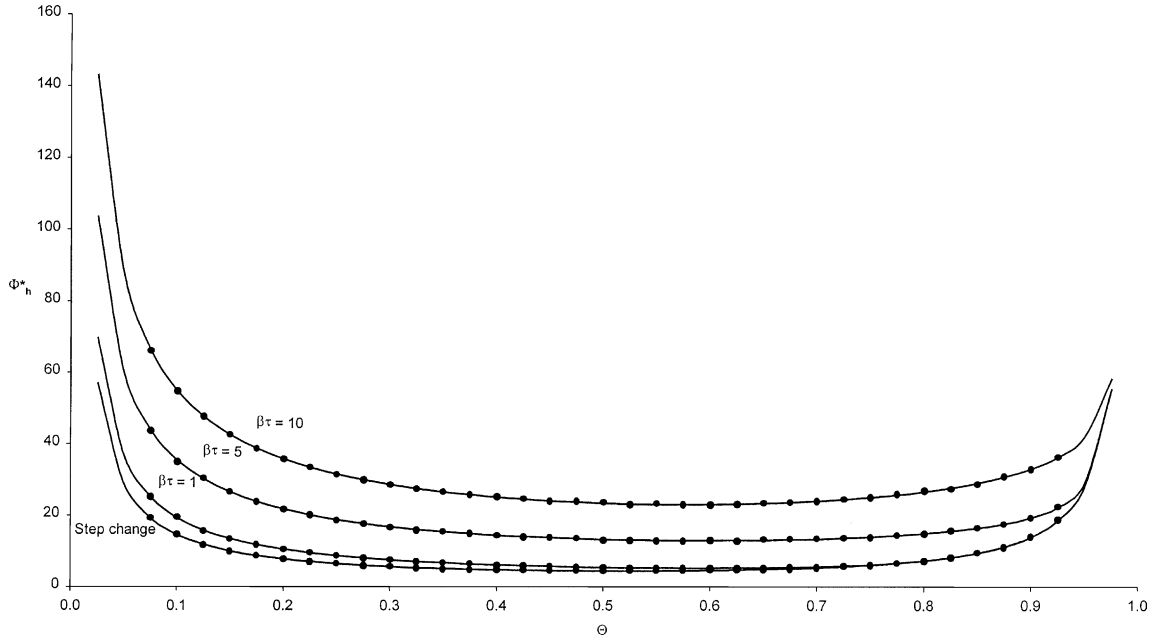


Fig. 4. Effect of  $\beta_\tau$  on variation of  $\Phi_h^*$  with  $\Theta$  for exponential case (symbols refer to computed values).

tainty,  $P_h$ , for a wide range of values of  $\Theta$  and  $\beta_\tau$ . For the computations,  $T_{aw} - T_0 = 40^\circ\text{C}$ ,  $P_T = 0.2^\circ\text{C}$  and  $h = 100\text{ W/m}^2\text{K}$ , which are typical of the values found in experiments with TLC. The excellent agreement between the computations and the theoretical values of  $\Phi_h^*$  gives confidence in the uncertainty analysis used here.

As pointed out in Section 2,  $\Phi_h^*$  provides an upper bound for the uncertainty in  $h$  even when the uncertainties in the temperatures are unequal. Fig. 4 is therefore important in showing how the uncertainties in  $h$  behave with  $\Theta$  and  $\beta_\tau$ . It can be seen that the step-change case (where  $\beta_\tau = 0$ ) provides the lower bound for  $\Phi_h^*$ , and this limit is approached for  $\beta_\tau < 1$ .

The minimum value of  $\Phi_h^*$  occurs for  $0.5 < \Theta < 0.6$ , depending on  $\beta_\tau$ . This is the range of  $\Theta$  in which experiments with TLC should be conducted if the uncertainties in  $h$  are to be kept to a minimum.  $\Phi_{h,\min}^*$  increases as  $\beta_\tau$  increases: for  $\beta_\tau = 1$ ,  $\Phi_{h,\min}^* \approx 5$ ; for  $\beta_\tau = 10$ ,  $\Phi_{h,\min}^* \approx 23$ . It therefore makes sense to design an experimental rig that makes  $\tau$  as small as practicable.

### 3.3. Exponential series

Using Eqs. (2.1) and (2.16),

$$\Gamma_\beta^{-1} = \sum_{j=1}^m c_j \beta \frac{\partial}{\partial \beta} [g(\beta, \lambda_j)] \quad (3.6)$$

and from Eq. (2.14),

$$\Gamma_h^{-1} = \sum_{j=1}^m c_j \Phi_{h,j}^{-1}, \quad (3.7)$$

where

$$\Phi_{h,j}^{-1} = \Gamma_\beta^{-1} \beta \frac{\partial}{\partial \beta} [g(\beta, \lambda_j)]. \quad (3.8)$$

That is,  $\Phi_h^{-1}$  is the sum of the weighted  $\Phi_{h,j}^{-1}$  components. When  $m = 1$ ,  $c_j = 1$  and  $\Phi_h$  is the same as that given in Section 3.2.

For the special case where the temperature uncertainties are equal,

$$\Phi_h^{*-1} = \sum_{j=1}^m c_j \Phi_{h,j}^{*-1} \quad (3.9)$$

and Fig. 4 can be used to show the variation of  $\Phi_{h,j}^*$  with  $\Theta$ .

## 4. Conclusions

Using solutions of Fourier's equation for a semi-infinite wall, analytical expressions have been derived for the amplification factor,  $\Phi_h$ , which relates the uncertainty in  $h$  to the uncertainties in the measured temperatures. Results have been obtained for the cases where the change of air temperature with time can be represented by: (i) a step change; (ii) a simple exponential; (iii) a series of exponentials. Cases (ii) and (iii) are referred to here as "slow transients". Excellent agreement was achieved between the analytical solutions for  $\Phi_h$  and values computed using a Monte Carlo method for the special case where the uncertainties in the measured temperatures are equal to each other. This special case provides an upper bound for  $\Phi_h$  when the uncertainties in the temperatures are unequal.

The results show that  $\Phi_h$  will be a minimum for all three cases when the nondimensional temperature,  $\Theta$ , is between 0.5 and 0.6. For the case of an exponential rise in air temperature,  $\Phi_{h,\min}$  increases as  $\beta_\tau$  increases, where  $\beta_\tau$  is a nondimensional heat transfer coefficient. These results should provide useful guidance for experimenters in the selection of design parameters for a rig and for the calculation and minimisation of the uncertainty in  $h$ .

### Acknowledgements

The authors wish to thank the Engineering and Physical Sciences Research Council (EPSRC) and Al-

stom Power Ltd for funding the research presented in this two-part paper.

### References

- Coleman, H.W., Steele, W.G., 1999. Experimentation and uncertainty analysis for engineers. Wiley, New York.
- Newton, P.J., Yan, Y., Stevens, N.E., Evatt, S.T., Lock, G.D., Owen, J.M., 2003. Transient heat transfer measurements using thermochromic liquid crystal. Part 1: An improved technique, *Int. J. Heat Fluid Flow* 24, 14–22.
- Yan, Y., Owen, J.M., 2002. Uncertainties in transient heat transfer measurements with liquid crystal. *Int. J. Heat Fluid Flow* 23, 29–35.